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Original Article



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Estimating the Drying Kinetics and Effective Moisture Diffusivity of Fresh Water Prawn (*Macrobrachium rosenbergii*)

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Abstract

Fresh-water prawn (*Macrobrachium rosenbergii*) once harvested, tends to deteriorate rapidly because of the high systemic moisture it constituent which has lead to post-harvest losses, drying as a method of preservation widely used for high moisture bio-products reduces moisture probably to bone-dry level and thereby increased the shelf-life of the fresh-water prawn. Therefore, Estimating the Drying Kinetics and Effective Moisture Diffusivity of Fresh Water Prawn (*Macrobrachium rosenbergii*) was investigated using a laboratory convective oven dryer and was arranged in a thin layer. 50-100°C temperatures were applied, varying on multiple of 10°C. It was observed that the drying rate increased with increasing drying temperatures. Drying data obtained were fitted into four empirical thin-layer drying models, and the best model was investigated after undergoing statistical parameters (of coefficient of determination, R2; root mean square error, RMSE and reduced chi-square, χ^2). The ANN and Henderson model was found to perform satisfactorily in describing the drying behaviour of the Fresh-water prawn samples at the chosen temperature levels. The initial moisture content of all the samples was 54% wb. The final effective moisture diffusivity of the samples during the drying experiments ranges from 1.26 x 10⁻⁷m²/s - 7.06 x 10⁻⁷m²/s, and the temperature related activation energy of diffusion was found to be 12.82-kJ/mol. Drying occurred mainly in the falling rate period, and the characterizing drying curves were exponential with increase in drying temperatures.

Keywords: Fresh-water prawn; Thin-layer drying; Drying kinetics; Modelling, effective; Diffusivity; Activation energy.

1. Introduction

Fresh-water prawn (*Macrobrachium rosenbergii*) are highly nutritious in protein, lipids and has a unique taste, it is low in cholesterol and highly demanded in national and international market. Prawn and shrimps are relatively cheap and available for consumption; they are good sources of animal protein for low income earners [1]. Prawns are endowed with both organic and inorganic contents. The essential constituents are proteins, carbohydrates and lipids, it contains a reasonable and significant proportion of minerals such as Ca, Mg, P, Mn, and Cl and vitamins such as A, C, and D [2]. Many researchers have also reported on the growth and nutritional composition of Fresh-water prawn under different culture conditions [3-8].

Shell-fish generally contain reasonable sources of nutrient in the maintenance and growth of human body [9].

Crabs and Prawn are highly perishable because of high systemic moisture it constitutes with low convective cell and high amino acid content.

Bangladesh reflect one of the most appropriate countries in the world for giant fresh water crayfish (*Macrobrachium rosenbergii*) due to it favourable resources and agro-climatic situation, it has a unique opportunity for the production of prawn [10] and prawn is very important in Basgladesh because it boast their national economy.

Once harvested, Fresh-water prawn (*Macrobrachium rosenbergii*) tends to quickly degenerate into spoilage due to the presence of high level of constituent water, proteins and certain mucilaginous matter. Spoilage is generally undesirable as it results in severe post-harvest losses and withdrawal from human consumption. Drying is a widely used practice in post-harvest preservation of such high moisture agricultural products. It is used to decrease moisture content possibly to skin-dry level which goes to reduce or even halt physiological and other microbiological activities that cause food rancidity and decay, thus, enabling storability of the product under ambient temperatures. Well-dried agricultural products are also reported to have long shelf-life in food packaging, lower transportation, handling, and storage costs [11-13]. See Plate 1.1.

Diffusion is the major phenomena that defines the simultaneous heat and mass transfer concept that consequently results in drying. It is a complicated process causing transfer of moisture from inside the food material to the air-food interface, and from this interface to the surrounds by convection [14, 15]. Drying time and prediction of suitable drying conditions for a particular product can be deduced using the empirical and semi-empirical thin layer drying models. This would also create a good data base for obtaining generalized drying curves and improve equipment design in the drying processes. However technical literature is very silent in the drying kinetics of Fresh-

water prawn (Macrobrachium rosenbergii). Objectives of this work therefore, are to estimate the drying kinetics and effective moisture diffusivity of Fresh Water Prawn (Macrobrachium rosenbergii) and to fit experimental data obtained at each of the chosen drying temperatures to some thin-layer models as to select the suitable drying model for the Fresh-water prawn (Macrobrachium rosenbergii).



Plate-1.1. A Fresh-water prawn (Macrobrachium rosenbergii)

2. Materials and Method

A large quantity of freshly Fresh-water prawn (Macrobrachium rosenbergii) was obtained from a local market at Ondewari community in Bayelsa State, Nigeria. The bulk was thoroughly washed to remove debris and stored in a refrigerator in the Processing Laboratory of the Department of Agricultural and Environmental Engineering, Niger Delta University, Bayelsa State, Nigeria. Samples were then taken from the bulk for the drying experiments. Initial moisture content of each set of five replicate samples (45-g each) was determine using (Plate.2.1) the oven-drying method with the temperature of the oven (WTC binder oven Model WTCB 1718). Equal thickness of the sample was 0.010-m using vanier claiper see Plate 2.2. All weight measurements were done using a laboratory-type digital balance with 0.01-g precision see Plate 2.3. An initial moisture content of about 54% wb was obtained by averaging the five replications. Thin-layer drying experiments were conducted at five levels of temperature (60, 70, 80, 90 and 100°C) and on five replications and average values of the final moisture content fixed at about 12-% db was reached. Weighing of the samples was continued, monitored at time intervals of 10-munites until no discernable change of weight was observed between the five replicates as described in Zibokere and Egbe [16] on red head palm weevil larvae, and Sankat and Mujaffar [17] on catfish. The drying data obtained at the falling rate period of drying were then worked into dimensionless moisture ratios (MR) based on Sahey and Singh [18].





Plate-2.2. A picture of Venier caliper



Plate-2.3. Laboratory-type digital balance with 0.01-g precision



$$MR = \frac{M - M_e}{M_o - M_e}$$

where

 M_e = equilibrium moisture content (emc), kg_{H_2O}/kg_{solid}

 M_o = initial moisture content, kg_{H_2O}/kg_{solid} .

However, for a rather cylindrical geometry of the crayfish samples, it was desired to obtain the equivalent moisture ratios by transformation using the Fick's second law diffusion equation as Guine, et al. [19] Chen, et al. [20].

$$MR = \frac{M - M_e}{M_0 - M_e} = \frac{8}{\pi^2} \int_{n=1}^{\infty} \frac{1}{n^2} e^{-(n)^2 \frac{\pi^2 D_e t}{L^2}}$$

where MR is dimensionless

n denotes the number of terms in the series (0, 1, 2, 3, ...),

t is drying time,

 D_e is effective moisture diffusivity (m² s⁻¹)

L relates to the geometric diameter, d_c of the samples [21].

 $d_{c} = (L \times W \times T)^{\frac{1}{3}}$

The factor, d_c is the dimensional estimator for L (length), W (width) and T (thickness) being the major, intermediate and minor diameters of the crayfish sample. Then Equation 2 will now give as Guine, et al. [19].

MR =
$$0.8106 \int_{n=1}^{\infty} \varepsilon_n^{-2} e^{-9.87\varepsilon_n (\frac{2e}{r_c^2})}$$
 3

where $\varepsilon_n = n^2$ seen as the root of a related Bessel function in terms of n

 $r_{\rm c}~=~geometric$ radius of the crayfish, and

 $(\frac{D_e t}{r_c^2})$ can be recognized as a Fourier factor.

For a long period of drying time (t $\approx \infty$), Equation 3 will tend to converge on the integration operation. The first term seems dominating for high drying time as required in thin-layer drying of products of cylindrical dimensions; thus rendering other terms in the series small enough to be ignored to give Equation 4 [22-24],

$MR = 0.8106e^{-9.87(\frac{D_e l}{r_c^2})}$	4
Taking natural log on both sides, equation 4 will linearize to	
$\ln(MR) = -(47D_{e}(\frac{1}{R_{c}})^{2}t + 1)$	5

2.1. The Effective Moisture Diffusivity, D_e

Drying parameter can be estimated from the slope of the plot when Equation 5 is plotted on a logarithmic scale (known as the slope method), as follows [19].

$$D_{e} = -slope \frac{[r_{c}^{2}]}{47}$$

2.2. Fitting to Thin-layer Drying Models

Data obtained from the drying experiments were fitted to seven thin-layer drying models as detailed below – Lewis model 7

 $MR = e^{-kt}$ [25] **Henderson-Parbis model** $MR = ae^{-kt}$ [26] Page model

1

8

 $MR = e^{-kt^n}$ [27] where

k is the kinetic (drying) rate constant and a, b, n are model constants.

The fitted models were each regressed using the nonlinear least squares regression method [28]. And by using SPSS 17.0 Microsoft Excel software, the experimental data used in the fitting were processed to statistical indicators such as coefficient of determination, R^2 , the reduced chi-square, χ^2 , mean bias error MBE, and the root mean square error, RMSE. These were used as indicators in selecting the best drying model. Following the procedure in Ndukwu, *et al.* [29] and Burubai [22] the statistical indicators were evaluated as follows

$$R^{2} = 1 - \left[\sum_{i=1}^{n} (MR_{pre,i} - MR_{exp,i})^{2}\right]$$

$$PMSE = \sqrt{\sum_{i=1}^{n} (MR_{pre,i} - MR_{exp,i})^{2}}$$
11

$$\chi^{2} = \frac{\sum_{i=1}^{n} (MR_{pre,i} - MR_{exp,i})^{2}}{n-k}$$
12

$$MBE = \left[\sum_{i=1}^{n} (MR_{pre,i} - MR_{exp,i})^2\right]$$
where
13

 $MR_{pre.}$ = predicted moisture ratio

 $MR_{exp.}$ = experimental moisture ratio

n = number of observations

k is as previously defined.

The set decision rule was that the model with the highest R^2 value, and the least χ^2 and RMSE values was selected as the best fit in describing the drying characteristics of the Fresh-water prawn (*Macrobrachium rosenbergii*) samples [30-32].

2.3. Activation Energy, E_a

The energy that is required to initiate molecular diffusion to cause drying in biomaterials is referred to as activation energy. Since in this work temperature, t is a measurable parameter, an Arrhenius type function was used to estimate the activation energy as Saxena and Dash [33] Da Silva, *et al.* [34].

$D_e = D_o(e^{-Ea/Rt})$	14				
where					
$E_a = activation energy, kJ/mol$					
$D_e = effective diffusivity at t^{o}K, m^{2}/s.$					
$D_o = pre-exponential factor of the Arrhenius equation at 0°K, m2/s.$					
R = universal gas constant (8.314 x 10-3, kJ/mol.K).					
t = air temperature expressed in °K					
Simplification of Equation 14 gives					
$\ln D_e = \ln D_o - \frac{E_a}{R} t^{-1}$	15				
or $-\frac{E_a}{R}t^{-1} = \ln D_e - \ln D_o$	16				
$\frac{E_a}{Rt} = \ln(\frac{D_o}{D_e})$	17				
$\frac{E_a}{R}t^{-1} = \ln(\frac{D_o}{D_e})$	18				
Plotting of $\ln D_e$ as a function of t ⁻¹ with regression line of slope, z (Fig. 1) that can be given as;					
$z = -\frac{E_a}{R}$ (as in Equation 19)	19				
whence, the activation energy can be estimated as Taheri-Garavanda, et al. [35], Navneet, et al. [36].					
$E_a = -zR$	20				

3. Results and Discussion

Figure 1 presents changes in moisture ratio with drying time of the Fresh-water prawn (Macrobrachium rosenbergii). As with literature report on drying of visco-elastic materials (such as the sea foods) the drying environment had significant effect on the moisture migration from the interior to the exterior in the drying of the Fresh-water prawn samples as expected [22, 32, 37, 38]. The figure 1 shows that on the same state of drying indicated by the moisture ratio, drying time increased greatly with drying temperature. This indicates that rate of moisture depletion during drying is significantly a function of drying time.

Figure-1. Moisture ratio versus drying time of Fresh-water prawn (Macrobrachium rosenbergii) at different drying temperatures



The drying curves in Fig. 2 depict the general trend of characteristic drying curves as reported for many biomaterials. The curves present initial steeper slope, and become asymptotic to the axis of drying time even with changing drying temperatures. This form adequately describes a more rapid initial moisture loss, and as moisture available for evaporation at the surface of the samples become lesser in drying [16, 17, 22, 38, 39].



3.1. Fitting Experimental Data into Thin-Layer Drying Models

Table 1 and 2 summarizes the statistical results from the thin-layer drying models for the different drying temperatures chosen in this work. The model with the highest R^2 value, and the least χ^2 and RMSE values was the criteria applied in selecting the best model describing the thin-layer drying characteristics of Fresh-water prawn (Macrobrachium rosenbergii). The fitting statistical results in the Tables showed that the coefficient of determination, R² values were consistently high in all the models. The shows that the R² in Henderson-pabis model ranging from 0.9986-.9326, RMSE values ranging from 0.004015-0.03035, χ^2 0.0000163-0.000228 while Page model R² has 0.7515-0.9965, RMSE 0.1741-0.006403 and χ^2 ranges from 0.01054-0.000041 and Lewis model R² ranges from 0.9833-0.9439, RMSE 0.0139-0.03608 and χ^2 0.00033-0.014316, Artificial Neural Network ANN, has R^2 is 0.9999 and χ^2 0.0000000000043 -0.000000003, RMSE has 0.000000367-0.0000548 as shown in table 1 and 2. This simply indicates the suitability of these empirical models in describing drying behavior Fresh-water prawn. However, when further tuned alongside the other statistical parameters, the model expression of ANN followed by that of the Henderson-pabis model gave the highest R^2 values and the lowest χ^2 and RMSE values in the temperature range of the work. However, Fig. 3 and 4 compared experimental data with data predicted with the ANN and Henderson-pabis model respectively at the chosen drying temperatures. It was observed that the value of k (kinetic rate constant with coefficient of determination, $R^2 = 0.9999$) increased with decrease in the drying temperatures indicating a steady drying rate suitable for good drying stability of the product without case-hardening. And the clustering of the moisture ratio values along the straight line, further indicated the suitability of ANN and Henderson-pabis model in describing drying characteristics of Fresh-water prawn (Macrobrachium rosenbergii) samples, similar in trend as observed by Darvishi, et al. [32] for shrimp.

Figure-3. Showing graph experimented moisture ratio against prediction moisture ratio for Fresh-water prawn (Macrobrachium rosenbergii) at 50°C



Figure-4. Showing graph experimented moisture ratio against prediction moisture ratio for Fresh-water prawn (*Macrobrachium rosenbergii*) at 50°C



 Table-1. Statistical Measures of Fresh-water prawn (Macrobrachium rosenbergii) on Thin-layer Drying Models Using Hendeson-pabis, Lewis and Page Model

	Model	TEMP°C	R ²	X ²	RMSE	MBE	Α	Ν	K
		50	0.9986	0.0000163	0.004015	0.0014	1.6307		0.0029
		60	0.9743	0.000303	0.017199	0.025735	2.1924		0.0049
		70	0.9329	0.000946	0.030535	0.067132	2.6886		0.0075
HENDERSON		80	0.9895	0.000228	0.002205	0.010509	1.8683		0.0065
MODEL									
		90	0.9892	0.00046	0.002337	0.010811	2.3941		0.0095
		100	0.9849	0.000471	0.003779	0.0151	2.9359		0.017
PAGI	E MODEL	50	0.9063	0.01054	0.011006	0.09374		1.461	0.0000982
		60	0.9965	0.000041	0.006403	0.0035		1.575	0.00007401
		70	0.9645	0.0005	0.022206	0.036		1.629	0.0000953
		80	0.8491	0.003281	0.056667	0.1509		1.592	0.000133
		90	0.8023	0.004493	0.09992	0.1977		1.636	0.000145
		100	0.7515	0.00776	0.1741	0.2485		1.56	0.000543
LEW	IS	50	0.9833	0.000195	0.01387	0.0167			0.001
MOD	EL								
		60	0.97163	0.00033	0.018057	0.02837			0.004
		70	0.9616	0.00054	0.02309	0.03839			0.007
		80	0.9645	0.000773	0.0275	0.03556			0.006
		90	0.9489	0.001161	0.033697	0.05109			0.009
		100	0.957	0.014316	0.036076	0.04295			0.017

Table-2. Statistical Measures of Fresh-water Prawn on Thin-layer Drying Models Using Artificial Neural Network, ANN						
	TEMP°C	MBE	R ²	X ²	RMSE	
	50	2.076E-09	0.9999	2.38E-11	0.00000488	
	60	8.207E-10	0.9999	4.3E-13	0.000000971	
	70	3.323E-09	0.9999	4.62E-11	0.00000679	
	80	6.33E-12	0.9999	1.35E-12	0.00000367	
	90	3.83E-08	0.9999	8.52E-10	0.00002919	
	100	9.92E-08	0.9999	3.0E-09	0.0000548	

3.2. Estimation of Effective Moisture Diffusivity and Activation Energy

The logarithmic moisture ratio values, ln (MR) plotted as a function of inverse of drying time, t⁻¹ at the various drying temperatures (as in Fig. 5), was used in the estimation of effective moisture diffusivity in table 3. The almost flattened regression line showed that less energy was required to remove moisture at the higher drying temperature as the water molecules within the body matrix tend to become free moisture at the surface of the samples. Effective moisture diffusivity, D_e thus, increased with drying time and temperature. In this work the D_e values ranged from 1.26 x 10^{-7} m²/s - 7.06 x 10^{-7} m²/s with the related activation energy, E_a value of 12.82-kJ/mol, similar in trend as observed by Xiong, *et al.* [40] for porous foods; in the work of Zogzas, *et al.* [24]; Guochen, *et al.* [41] for shrimp and for fruits and vegetables [42].

Table-3. Mosisture diffusivity values of African Giant Snail (Achatina Achatina)

Temperature °C	Average effective moisture diffusivity
50	0.000000126
60	0.000000126
70	0.00000304
80	0.00000276
90	0.00000385
100	0.00000709



4. Conclusion

Drying kinetics was investigated for Fresh-water prawn (*Macrobrachium rosenbergii*) dried on thin layers at drying temperatures of 50 60, 70, 80, 90 and 100°C. As with other biological materials drying was observed to follow the falling rate period. The ANN followed by Henderson-pabis model was considered adequate and was selected as good estimator of the drying behaviour of the Fresh-water prawn (*Macrobrachium rosenbergii*) at the drying temperatures applied. In this work, the D_e values ranges from 1.26 x 10^{-7} m²/s - 7.06 x 10^{-7} m²/s with the related activation energy, E_a value of 12.82-kJ/mol following an Arrhenius relationship reduces to the slope method and fall within the values in technical literature over same temperature range of this work. The effective moisture diffusivity also increased in value with increased drying temperatures.

Conflict of Interest

There is no potential conflict of interest on this work.

References

- [1] Adeyeye, E. I., 1996. "Waste yield, proximate and mineral composition of three different types of land snails found in Nigeria." *International Journal of Food Science and Nutrition*, vol. 47, pp. 111-116.
- [2] Abulude, F. O., Lawal, L. O., Ehikhamen, G., Adesanya, W. O., and Ashafa, S. L., 2006. "Chemicalcomposition and functional properties of some prawns from the coastal area of Ondo state, Nigeria." *Electron Journal of Environment, Agriculture and Food Chemistry*, vol. 5, pp. 1235-1240.

- [3] Gomez, G. H., Nakagawa, and Kasanara, S., 1988. "Effect of dietary protein/ starch ratios and energy level on growth of the giant freshwater prawn, Macrobrachium rosenbergii." *Nippon Suisan Gakkaishi*, vol. 54, pp. 1401-1407.
- [4] Reed, L. and Abramo, L. R. D., 1989. "A standard reference diet for crustacean nutrition research III. Effects on weight gain and amino acid composition of whole body and tail muscle of juvenile prawns Macrobrachium rosenbergii." *Journal of World Aquaculture Society*, vol. 20, pp. 107-113.
- [5] Sheen, S. S. and D'Abramo, L. R., 1991. "Response of juvenile freshwater prawn, Macrobrachium rosenbergii to different levels of cod liver oil/ corn oil mixture in semi purified diet." *Aquaculture*, vol. 93, pp. 121-134.
- [6] Hossain, M. A. and Paul, L., 2007. "Low-cost diet for monoculture of giant freshwater prawn Macrobrachium rosenbergii (de Man) in Bangladesh." *Aquaculture Research*, vol. 38, pp. 232-238.
- [7] Hossain, M. A., Siddique, M. A. L., and Miaje, M. A. H., 2006. "Development of low cost feed for culture of giant fresh water prawn Macrobrachium rosenbergii de Man in ponds." *Bangladesh Journal of Fisheries*, vol. 4, pp. 127-134.
- [8] Habashy, M. M., 2009. *Growth and body composition of juvenile freshwater prawn, Macrobrachium rosenbergii, fed different dietary protein/starch ratios.* Cairo, Egypt: National Institute of Oceanography and Fisheries, Fish Research Station, El-Qanatar El-Khairya.
- [9] Dong, F. M., 2001. *The nutritional value of shellfish*. A Washington Sea Grant Programme Publication, p. 8.
- [10] Ahmed, N., Demaine, H., and Muir, J. F., 2008. "Freshwater prawn farming in Bangladesh: history, present status and future prospects." *Aquacul. Res.*, vol. 39, pp. 806-819.
- [11] Unal, H. G. and Sacilik, K., 2011. "Drying characteristics of hawthorn fruits in a convective hot-air dryer." *Journal of Food Processing and Preservation*, vol. 35, pp. 272-279.
- [12] Yu, H., Zuo, C., and Xie, Q., 2015. "Drying characteristics and model of chinese hawthorn using microwave coupled with hot air." *Mathematical Problems in Engineering*, vol. 2015, Available: <u>https://doi.org/10.1155/2015/480752</u>
- [13] Doris, T. H., 2016. "Seafood safety and quality: The consumer's role." *Foods*, vol. 5, pp. 71-93.
- [14] Menges, H. O. and Ertekin, C., 2006. "Mathematical modelling of thin layer drying of Golden apples." *Journal of Food Engineering*, vol. 77, pp. 119-125.
- [15] Yi, X. K., Wu, W. F., Zhang, Y. Q., Li, J. X., and Luo, H. P., 2012. "Thin-layer drying characteristics and modelling of Chinese jujubes." *Mathematical Problems in Engineering*, vol. 2012, Available: <u>https://doi.org/10.1155/2012/386214</u>
- [16] Zibokere, D. S. and Egbe, E. W., 2019. "Thin-layer Drying Kinetics of Palm Weevil (Rhynchophorus ferruguneus) Larvae." *Annals of Applied Science*, vol. 5, pp. 40-46.
- [17] Sankat, C. K. and Mujaffar, S., 2006. "Modelling the drying behaviour of salted catfish fillets." In 15th International Drying Symposium (IDS 2006), Budapest Hungary, 20 23 August.
- [18] Sahey, K. M. and Singh, K. K., 2005. *Unit operations in agricultural processing*. 2nd ed. New Delhi: VIKAS Publishing PVT Ltd. pp. 125-130.
- [19] Guine, R. P. F., Pinho, S., and Barroca, M. J., 2011. "Study of the convective drying of pumpkin (Cucurbita maxima)." *Food Bio-production Process*, vol. 89, pp. 422-428.
- [20] Chen, J., Zhou, Y., Fang, S., Meng, Y., Kang, X., Xu, X., and Zuo, X., 2013. "Mathematical modelling of hot air drying kinetics of momordica charantia slices and its color change." *Advanced Journal of Food Science and Technology*, vol. 5, pp. 1214-1219.
- [21] Mohsenin, N. N., 1986. *Physical properties of plant and animal materials* vol. 1. USA: Gorgon Beach Science Publications.
- [22] Burubai, W., 2015. "Thin layer drying kinetics of fresh water clam (Tridacna maxima)." *Umudike Journal* of Engineering and Technology, vol. 1, pp. 79-90.
- [23] Babalis, S. J. and Belessiotis, V. G., 2004. "Influence of drying conditions on the drying constants and moisture diffusivity during the thin-layer drying of figs." *Journal of Food Engineering*, vol. 65, pp. 449-458.
- [24] Zogzas, N. P., Maroulis, Z. B., and Marinos-Kouris, D., 1996. "Effective moisture diffusivity estimation from drying data. A comparison between various methods of analysis." *Drying Technology*, vol. 14, pp. 1543-1573.
- [25] Bruce, D. M., 1985. "Exposed-layer barley drying, three models fitted to new data up to 150 °C." *Journal of Agricultural Engineering Research*, vol. 32, pp. 337-347.
- [26] Henderson, S. M. and Pabis, S., 1961. "Grain drying theory I: temperature effect on drying coefficient." *Journal of Agricultural Engineering Research*, vol. 6, pp. 169-174.
- [27] Vega-Gálvez, A., Miranda, M., Diaz, L. P., Lopez, L., Rodruguez, K., and Di Scala, K., 2010. "Effective moisture diffusivity determination and mathematical modelling of the drying curves of the olive-waste cake." *Bioresource Technology*, vol. 101, pp. 7265-7270.
- [28] Haydar, K., Aydin, K., and Adnan, M., 2014. *Common applications of thin-layer drying curve equations and their evaluation criteria*. Progress in Exergy, Energy, and the Environment, pp. 669-680.
- [29] Ndukwu, M. C., Ogunlowo, A. S., and Olukunle, O. J., 2010. "Cocoa bean (Theoboroma cacao) drying kinetics." *Chilean Journal of Applied Agriculture*, vol. 70, pp. 633-639.
- [30] Wang, Z., Sun, J., Liao, C. F., Zhao, G., and Wujand, H. U. X., 2006. "Mathematical modelling on hot air drying of thin layer apple pomace." *Journal of Food Engineering*, vol. 40, pp. 39-46.

- [31] Maydeu-Olivares, A. and Garca-Forero, C., 2010. "Goodness-of-fit testing." *International Encyclopaedia of Education*, vol. 7, pp. 190-196.
- [32] Darvishi, H., Farhang, A., and Hazbavi, E., 2012. "Mathematical modeling of thin-layer drying of shrimp." *Global Journal of Science Frontier Research*, vol. 12, pp. 83-89.
- [33] Saxena, J. and Dash, K. K., 2015. "Drying kinetics and moisture diffusivity study of ripe jackfruit." *International Food Research Journal*, vol. 22, pp. 414-420.
- [34] Da Silva, W. P., Rodrigues, A. F., Silva, C., De Castro, D. S., and Gomes, J. P., 2015. "Comparison between continuous and intermittent drying of whole bananas using empirical and diffusion models to describe the processes." *Journal of Food Engineering*, vol. 166, pp. 230-236.
- [35] Taheri-Garavanda, A., Rafieea, S., and Keyhania, A., 2011. "Effective moisture diffusivity and activation energy of tomato in thin layer dryer during hot air drying. International transaction." *Journal of Engineering, Management, and Applied Sciences and Technologies*, vol. 2, pp. 239-248.
- [36] Navneet, K., Sarkar, B. C., and Sharma, H. K., 2012. "Mathematical modelling of thin layer hot air drying of carrot pomace." *Journal of Food Science and Technology*, vol. 49, pp. 33-41.
- [37] Ikrang, E. G., 2014. Development of a model for thin layer solar drying of salted fish fillets. Phd Thesis, department of agricultural and bioresources engineering. Nsukka: University of Nigeria.
- [38] Jain, D. and Pathare, P., 2007. "Studying the drying kinetics of open sun-drying of fish." *Journal of Food Engineering*, vol. 78, pp. 1315-1319.
- [39] Kilic, A., 2009. "Low temperature and high velocity (LTHN) application in drying: characteristic and effects on fish quality." *Journal Food Engineering*, vol. 91, pp. 173-182.
- [40] Xiong, X., Narsimhan, G., and Okos, M. R., 1992. "Effect of composition and pore structure on binding energy and effective diffusivity of moisture in porous foods." *Journal of Food Engineering*, vol. 15, pp. 187-208.
- [41] Guochen, Z., Arason, S., and Arnason, S. A., 2009. "Dehydration property of shrimp (Pandalus borealis) undergoing heat-pump drying process." *International Journal Agriculture and Biology Engineering*, vol. 2, pp. 92-97.
- [42] Daniel, I. O., Norhashila, H., Rimfiel, B. J., Nazmi, M. N., and Khalina, A., 2016. "Modelling the thin-layer drying of fruits and vegetables: A Review." *Comprehensive reviews in Food Science and Food Safety*, vol. 15, pp. 599-618.